

# **PETE 310**

## **Lecture # 20**

### **Properties from Reservoir Fluid Studies Report**

# Recall Nomenclature...

TABLE 10-3

## Nomenclature used in analysis of reservoir fluid studies

$B_{oD}$  = relative oil volume by differential vaporization, page 5, column 3, Table 10-1

$B_{oDb}$  = relative oil volume at bubble point by differential vaporization, page 5, column 3, Table 10-1

$B_{oSb}$  = formation volume factor at bubble point from separator test (at selected separator pressure), page 7, column 6, Table 10-1

$(V_t/V_b)_F$  = relative total volume (oil and gas) by flash vaporization, page 4, column 2, Table 10-1

$B_{tD}$  = relative total volume (oil and gas) by differential vaporization, page 5, column 4, Table 10-1

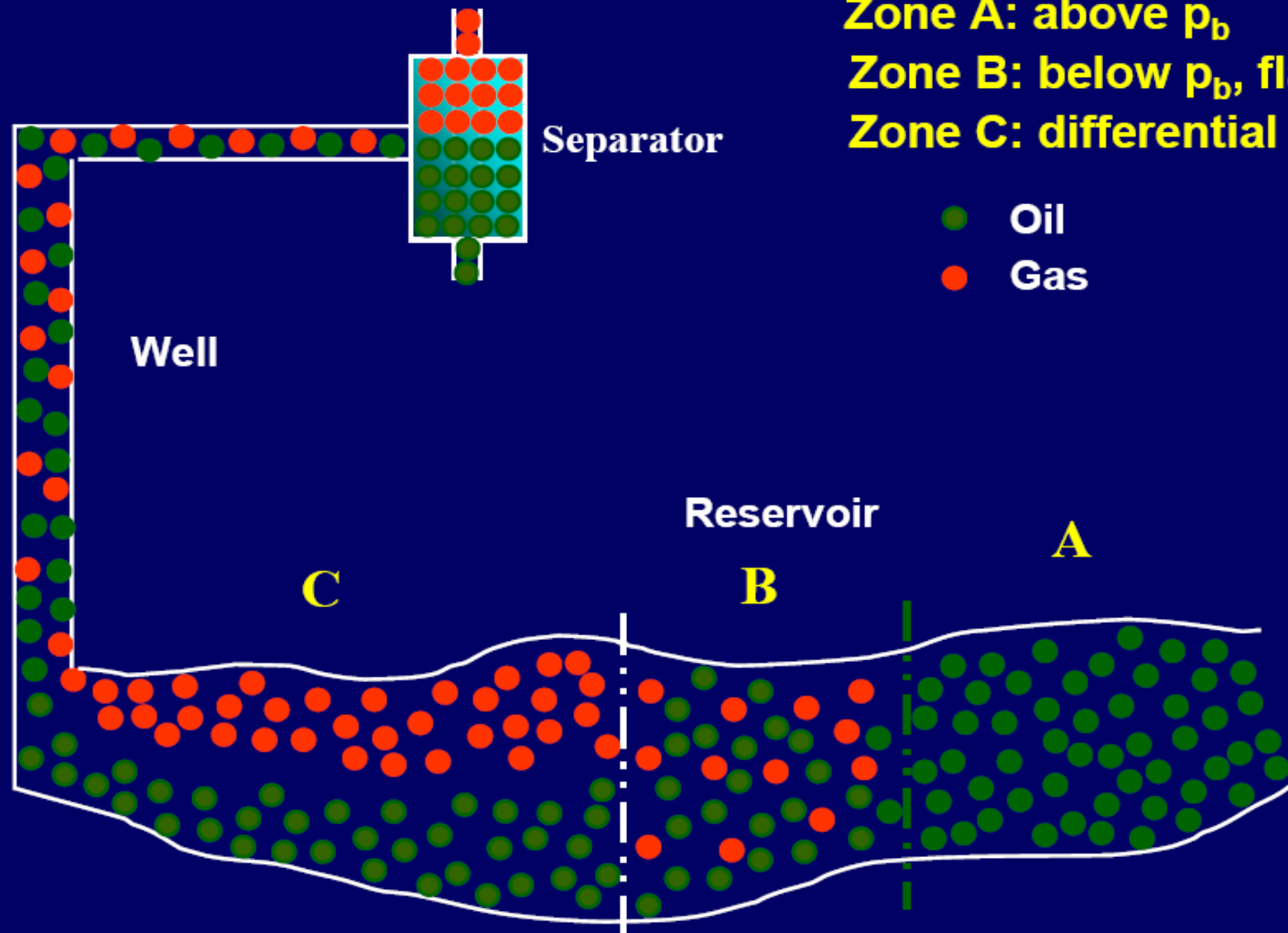
$R_{sD}$  = gas remaining in solution by differential vaporization, page 5, column 2, Table 10-1

$R_{sDb}$  = gas in solution at bubble point (and above) by differential vaporization, page 5, column 2, Table 10-1

$R_{sSb}$  = sum of separator gas and stock-tank gas from separator test (at selected separator pressure), page 7, column 4, Table 10-1

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# Phase transition in oil reservoir



# Assumptions

- For  $p > p_b$  fluid properties are computed by combining data from the CCE test and a separator test

$$B_o = B_{oSb} \left( \frac{V_t}{V_b} \right)_{CCE} \quad p \geq p_b$$

# Assumptions

- For  $p < p_b$  the process in the reservoir can be simulated from a DL test, the region from the bottom of the well to the stock tank can be represented by a separator test
- Thus fluid properties for  $p < p_b$  are computed by combining data from DL and separator tests

$$B_o = B_{oD} \frac{B_{oSb}}{B_{oDb}} \qquad R_s = R_{sD} \frac{R_{sSb}}{R_{sDb}}$$

**Note: Do not use expression for  $R_s$  in book – This is NEWER**

# Possible Exercises

- Given the following PVT reports determine
  - Isothermal compressibility at  $p=2200$  psi
  - Bubble point pressure

## Constant Mass Expansion at 150.0 F

Pressure psi	Rel Vol U/U <sub>b</sub>	Compressibility 1/psi	Y-factor
3500	0.9643	9.44E-06	
3000	0.9698	1.02E-05	
2500	0.9757	1.11E-05	
2000	0.9823	1.22E-05	
1500	0.9896	1.34E-05	
1000	0.9977	1.49E-05	
500	1.5053		1.45

# Possible Exercises

■ Given the following PVT reports determine

■  $B_o$  and  $R_s$  at  $p = 2000$  psi ( $> p_b$ )

## Constant Mass Expansion at 150.0 F

Pressure psi	Rel Vol U/U <sub>b</sub>	Compressibility 1/psi	Y-factor
3500	0.9643	9.44E-06	
3000	0.9698	1.02E-05	
2500	0.9757	1.11E-05	
2000	0.9823	1.22E-05	
1500	0.9896	1.34E-05	
1000	0.9977	1.49E-05	
Pb = 866	1.0000	1.54E-05	
500	1.5053		1.45

Fluid : TEST 3 PT 1 SEP LIQUID BOTTLE # K-6000  
Standard Characterization

## Differential Depletion at 150.0 F

Pressure psi	Oil Form Vol Fact Bod	Solution GOR (Rsd) Scf/bbl	Gas Form Vol Fact Bg	Res Oil Density lbm/ft <sup>3</sup>	Comp. Fact Z	Gas Gravity air=1
866	1.206			44.16		
Pb = 866	1.206	307.0		44.16		
600	1.165	223.2	0.026450	44.94	0.915	0.7638
400	1.134	160.4	0.040427	45.54	0.932	0.8164
200	1.097	90.2	0.082588	46.24	0.950	0.9526
100	1.071	44.6	0.167457	46.71	0.960	1.1696
14.7/60	1.000			49.17		

# Exercise

- Given the following reports determine
  - $B_o$  and  $R_s$  at  $p = 400$  psia ( $< p_b$ )

Fluid : TEST 3 PT 1 SEP LIQUID BOTTLE # K-6000  
Standard Characterization

## 1 Stage Separator Test

Pressure psi	Temp F	Gas Oil Ratio Scf/bbl STO	Gas Gravity Air = 1	Oil Density lbm/ft <sup>3</sup>	Formation Factor bbl/bbl STO
866	150.0			44.2	1.210
150	100.0	224.2	0.843	47.5	1.070
15	60.0	90.0	1.294	49.2	1.000

